# **Fabrication of Double Slope Solar Distillation System**

V.NARESH <sup>1</sup>	ASSOCIATE PROFESSOR	BHARATHIDASAN ENGINEERING COLLEGE
ARAVINDHAKUMAR.M <sup>2</sup>	PG STUDENTS	BHARATHIDASAN ENGINEERING COLLEGE
PRADEEPKUMAR P <sup>3</sup>	PG STUDENTS	BHARATHIDASAN ENGINEERING COLLEGE
SANTHOSHKUMAR.M <sup>4</sup>	PG STUDENTS	BHARATHIDASAN ENGINEERING COLLEGE
SATHIYARASU.G <sup>5</sup>	PG STUDENTS	BHARATHIDASAN ENGINEERING COLLEGE

### ABSTRACT

There is almost no water left on earth that is safe to drink without purification after 20-25 years from today. This is a seemingly bold statement, but it is unfortunately true. Only 1% of Earth's water is in a fresh, liquid state, and nearly all of this is polluted by both diseases and toxic chemicals. For this reason, purification of water supplies is extremely important. Keeping these things in mind, we have devised a model which will convert the dirty/saline water into pure/potable water using the renewable source of energy (i.e. solar energy). The basic modes of the heat transfer involved are radiation, convection and conduction. The results are obtained by evaporation of the dirty/saline water and fetching it out as pure/drinkable water. Its application was proven to be most economical, as most systems in individual uses requires. This paper reviews the present day solar thermal technologies. Performance analyses of existing designs (study), and fabrication of double slope solar distillation system have been discussed in this paper.

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#### I. INTRODUCTION

The sun radiates the energy uniformly in all direction in the form of electromagnetic waves. When absorbed by body, it increases its temperature. It is a clean, inexhaustible, abundantly and universally available renewable energy.

At the bottom side of the basin, 38 copper tubes of 1.5cm outer diameter were carefully arranged and submerged under three litter of tap water. Depending on the desired R-value, some of the tubes were filled with PCM and the remaining tubes were left empty. In each experiments, all the 38 tubes were always used and the only thing changes is the number of PCM filled tubes to investigate the effect of the amount of PCM on the water productivity. The PCM capacity of each tube is 40 g and the PCM filled tubes were tightly sealed to prevent water from leaking in or PCM from leaking out of the tubes. All tubes were painted with a black colour to maximize the solar irradiation absorption.



#### **Experimental procedure**

The experiments were carried out from April to August 2018 in Muscat-Oman. Each set of experiment was conducted within four consecutive days for the four desired values of the parameter R (0, 0.17, 0.35 and 0.51) which is defined as Mass of PCM Mass of Water. The experiments typically start from 8:30 a.m. until the next day 7:30 a.m. The collected water (condensate) was recorded every one hour until 12:00 a.m. and the accumulated water produced after 12 a.m. is recorded the next day morning. After each experiment, the pH and conductivity of the collected water were measured and recorded and the recorded temperatures data (basin water, ambient, PCM, and vapor) were extracted from the temperature recorder and analysed using excel. Table

1 shows the number of PCM filled tubes, mass of PCM and the value of R for eachs et of four experiments. The mass of the water is constant and equals 3kg and its electrical conductivity is  $869.6 \,\mu$ S/cm.

#### **Experimental Set-up**

The photograph of double slope active solar still under study have been shown in fig.2. In active solar still, the flat plate collector is integrated with double slope active solar still in such a way that the hot water from collector plate enters into the basin of solar still under forced circulation mode. The inlet and outlet connections to the collector plate are taken from the bottom of the basin as shown in Figure 1a. A gate valve has been provided in the inlet pipe to control the circulation of water through the collector plate. The collector plate absorbs the solar energy and transfers that energy to water flowing through tubes. The double slope solar still placed in east-west direction and collector plate was inclined at 300 facing south to



Table 5.2.1. Observation under Normal mode Drying



Day 1

Temp/Time	9am	10am	11am	12am	14pm	15pm	16pm
(Ambient)T <sub>1</sub>	31	32	34	36	35	31	30
(Inlet) T <sub>2</sub>	31	32	34	36	35	31	30
(Bed) T <sub>3</sub>	32	33	35	37	36	31	31
(outlet) T <sub>4</sub>	30	31	33	35	34	30	30
M(kg)							
chilli	1 kg						0.75

Chilli,

Intial Weight = 1 kg Final weight = 0.75 kg Moisture Removed = 0.25kg

Temp/Time	9am	10am	11am	12am	13pm
(Ambient)T <sub>1</sub>	30	33	34	35	37
(Inlet) T <sub>2</sub>	30	33	34	35	37
(Bed) T <sub>3</sub>	31	34	35	36	38
(outlet) T <sub>4</sub>	30	32	33	34	36
M(kg)					
chilli	0.75kg				

Chilli, Intial Weight = 1 kg Final weight = 0.55 kg Moisture Removed = 0.45kg

Day 3						
Temp/Time	9am	10am	11am	12am		
(Ambient)T <sub>1</sub>	31	32	35	37		
(Inlet) T <sub>2</sub>	31	32	35	37		
(Bed) T <sub>3</sub>	32	33	37	37		
(outlet) T <sub>4</sub>	30	31	33	35		
M(kg)						
chilli	0.55kg					

Chilli

Intial Weight = 1 kg Final weight = 0.33 kg Moisture Removed = 0.67kg

#### **Drier Efficiency Evaluation**

Mode	Sample weight, mg (kg)	Moisture Evaporated $m_W$ (kg)	Avg. Temp. Inlet(T <sub>2</sub> ) °c	Avg. Temp. outlet(T <sub>4</sub> ) °c	Avg. solar Insolation, (I) w/m <sup>2</sup>	Avg. sunshine hours, (t <sub>d</sub> )
Normal	1	0.67	34	33	800	6
Dual	1	0.66	35	31	750	6

## Variation of Drier Bed Temperatures (T<sub>3</sub>) vs Drying Time

The following graph shows the variation of temperature  $,T_3$  inside the drying cabinet and ambient temperature with Drying time in Normal and Dual modes. Increasing the temperature inside the cabinet will enhance drying rate and efficiency



Figure 5.4.1 Drier Bed Temperature vs Dying Time

#### II. CONCLUSION

The efficiency of the dual mode drying ( $\eta_{dth=21.1\%}$ ) gets increased compared to normal mode drying ( $\eta_{dth=19.6\%}$ )

The Drying time for the same quantity of grain(chilli) as found decreased from 22hrs to 16hrs.

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